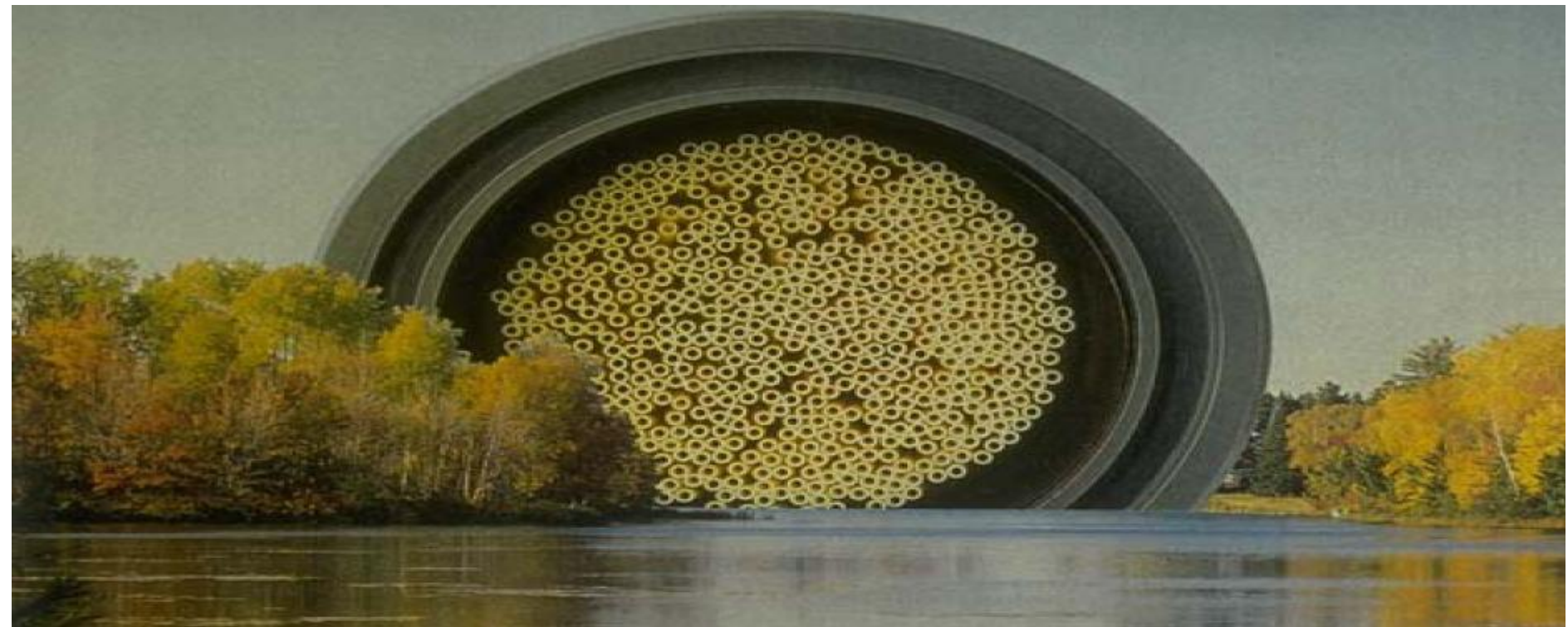


# ULTRAFILTRATION TECHNOLOGY



**By: Yaser Shirazi**  
**Nov.2012**

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- Introduction
- UF applications
- UF design parameters
- UF process
- UF modules
- CSM UF
- Conclusion

# Introduction

- What is UF technology?
  - Mechanism: Molecular sieve
  - Structure: Asymmetric
  - Driving force: Pressure
  - Pore size: 0.1-0.01  $\mu\text{m}$
  - Molecular weight cutt-off



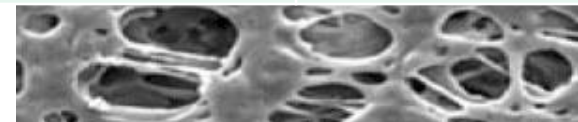
Ultra thine  
separate lyer

Support layer  
substrate

Polyester

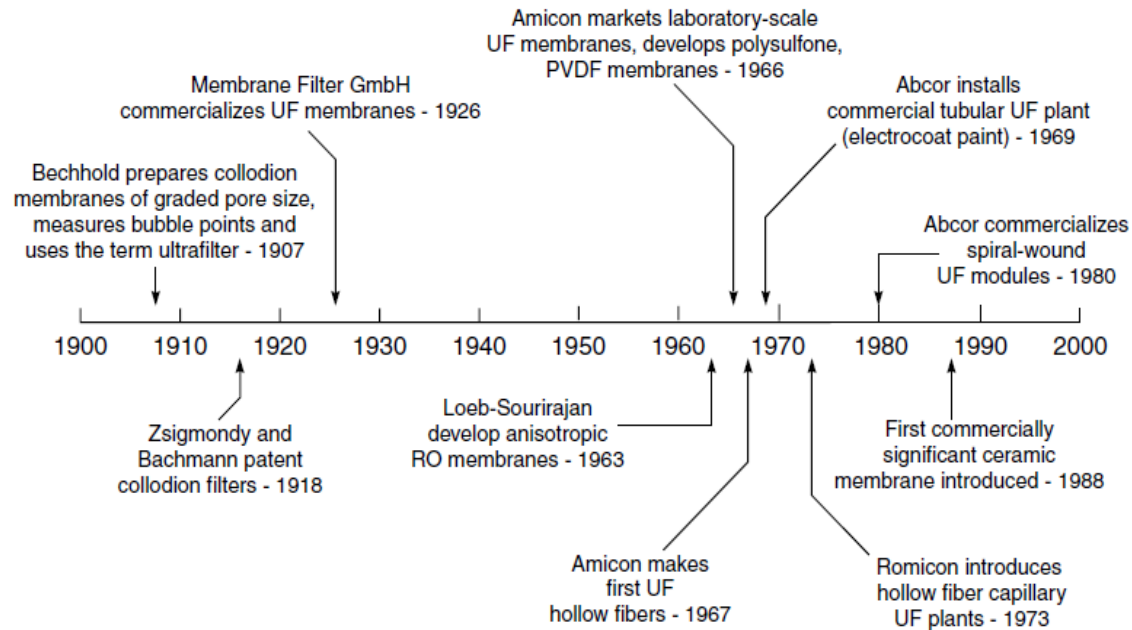


Nanofiltration	$10^2$ - $10^4$
Reverse osmosis	$10^2$

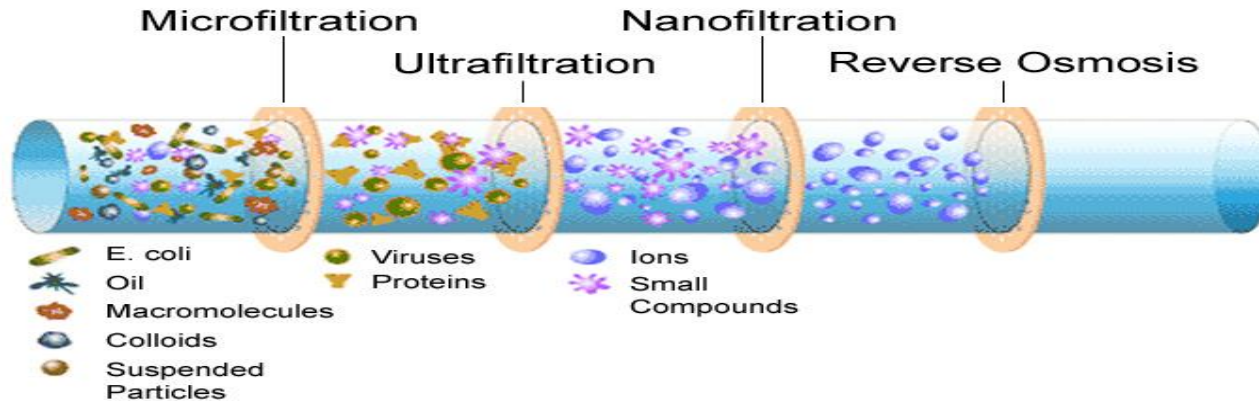
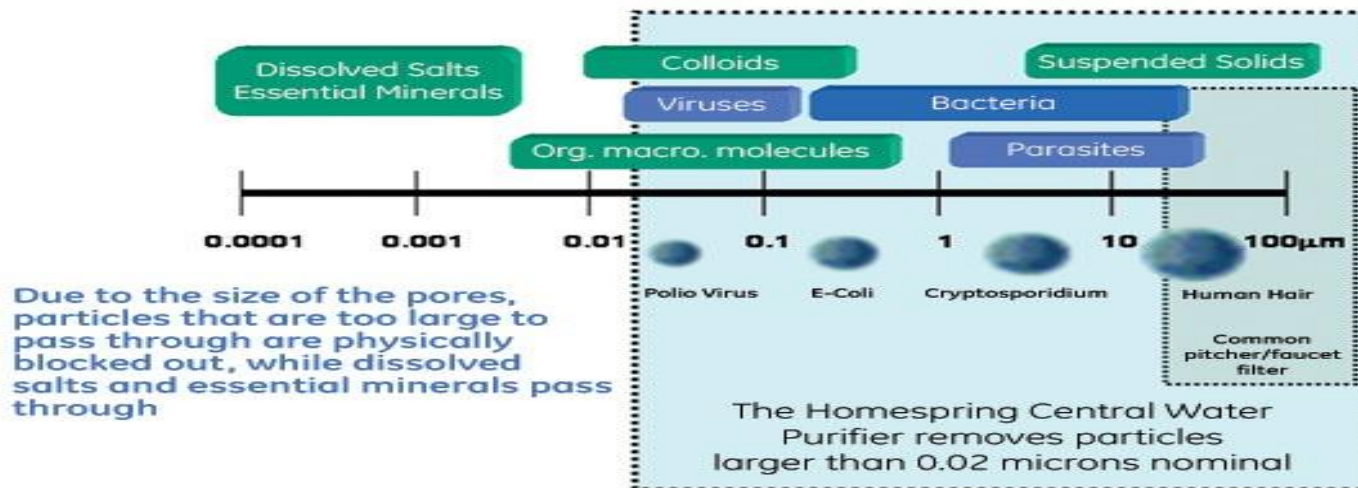


# Introduction

- History of UF



# UF removal ability



# Introduction

Filter type	Symbol	Pore Size, $\mu\text{m}$	Operating Pressure, psi	Types of Materials Removed
Microfilter	MF	1.0-0.1	<30	Clay, bacteria, large viruses, suspended solids
Ultrafilter	UF	0.1-0.01	20-100	Viruses, proteins, starches, colloids, silica, organics, dye, fat
Nanofilter	NF	0.01-0.001	50-300	Sugar, pesticides, herbicides, divalent anions
Reverse Osmosis	RO	< 0.0001	225-1,000	Monovalent salts

# Why UF?

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- Advantages
  - Low pressure
  - High permeation
  - Easy cleaning
  - Low cost
  - Low energy
  - Low spacing
  - High efficiency

# UF application

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- Pretreatment for Reverse Osmosis (RO) and DI system
- Post-treatment for micro-organism & turbidity removal for
  - Iron removal & de-mineralize process in underground water treatment
  - Water softening application
  - Ultra-pure process water for production and rinsing, i.e. food processing, laboratory, etc.
  - Drinking water and mineral water treatment
  - Secondary wastewater treatment for disposal
  - Recycling of wastewater as potable water.
- Separation/ purification & concentration for
  - Food & Beverages, dairy, wine and fruit juice industry
  - Pharmaceutical industries



# UF materials

- Ceramics
  - Comparatively fragile
  - Narrow operating pH range
  - Low flux
  - High chemical & thermal stability
- Polymers
  - Durability
  - High flux
  - Processability

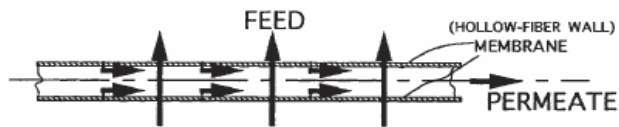


# UF polymer materials

- PVDF
  - strong and very tough material
  - resistant to abrasion, acids, bases, solvents and much more
  - usable to  $280^{\circ}F$  ( $138^{\circ}C$ )
  - usable in laboratory plumbing
- PES
- PS
  - rigid, high-strength
  - highly resistant to mineral acids, alkali
- PAN
- PP
  - lightweight
  - temperature up to  $180^{\circ}F$  ( $82^{\circ}C$ )
  - highly resistant to acids, bases and many solvents
  - usable in laboratory plumbing
- CA
  - Expensive
  - Low chemical resistant
  - High chlorine resistant
- PVC
  - strong and rigid
  - resistant to a variety of acids and bases
  - may be damaged by some solvents and chlorinated hydrocarbons
  - maximum usable temperature  $140^{\circ}F$  ( $60^{\circ}C$ )
  - usable for water, gas and drainage systems
  - not useable in hot water systems

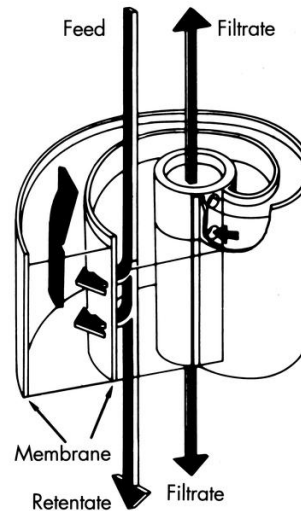
# UF modules

## Hollow fiber



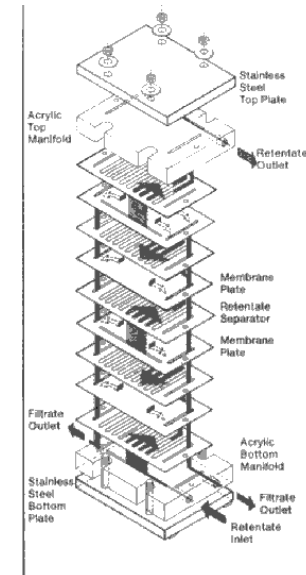
- High efficiency
- High packing density
- Susceptible to structural deformation
- Cleanable

## Spiral wound



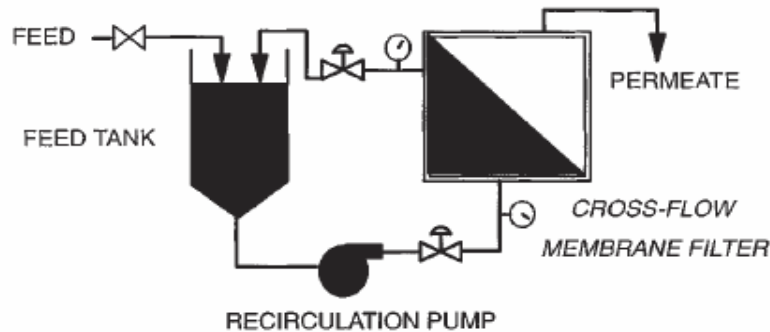
- Cannot produce turbulent flow with the flowrates at which we are operating
- Small footprint

## Cassette



- Produces turbulent flow for better medium-membrane communication.
- Small footprint
- Large membrane surface area

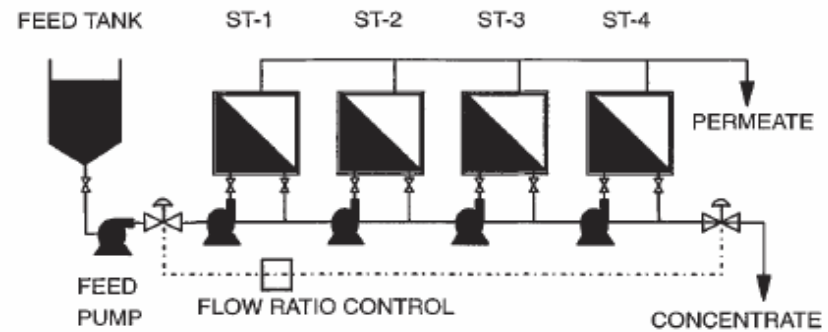
# Operation Set-up



## Batch, Semi-Batch Operation

tank volume and membrane area required.

-Conversion per pass is low, but with multiple passes, virtually any concentration can be achieved



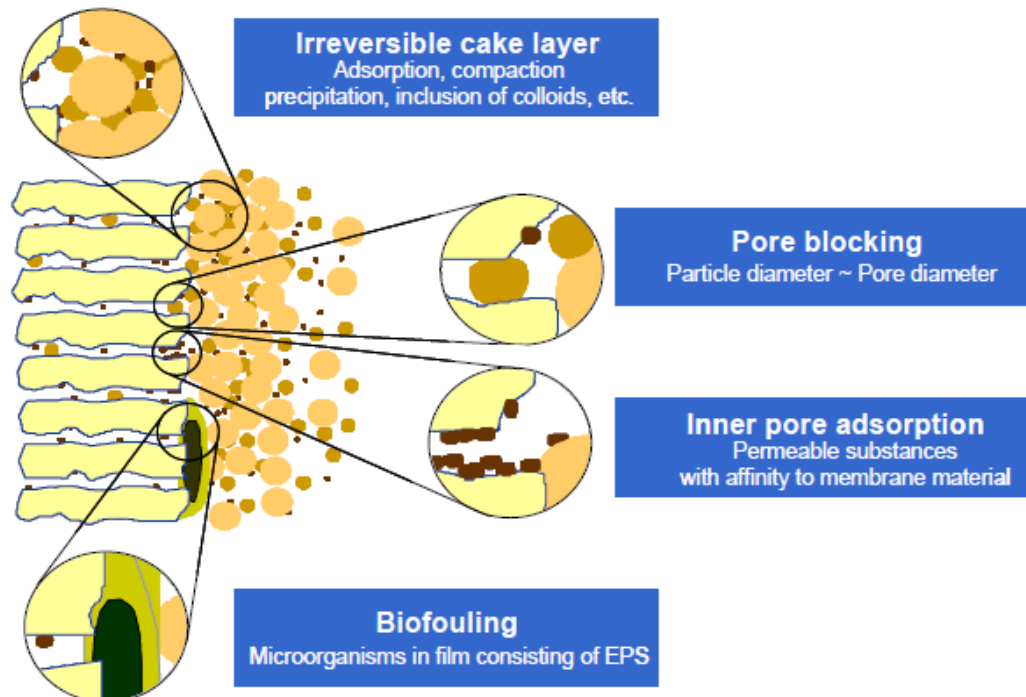
## Series Operation

-Fresh medium continually added to feed tank

-Continual re-pressurization require

# Fouling

- Permeability reduction
- Plants, algae, microorganism and humic acids
- Solutions:
  - Backwash
  - CEB
  - CIP



# UF theory

- **Mass balance**

- Feed= Filtration + cleaning+ concentrate

- **Recovery**

- $R = [\text{feed} - (\text{filtered volume} + \text{cleaning volume})] / \text{feed}$

- **Kinetics**

$$J = Q_p / A_{\text{mem}} = \text{TMP} / (v \cdot R_{\text{tot}})$$

$J = \text{flux} [m^3 / (m^2 \cdot h)]$

$Q_p = \text{permeate flow} [m^3 / h]$

$A_{\text{mem}} = \text{membrane surface area} [m^2]$

$\text{TMP} = \text{transmembrane pressure} [Pa]$

$R_{\text{tot}} = \text{totale resistance}$

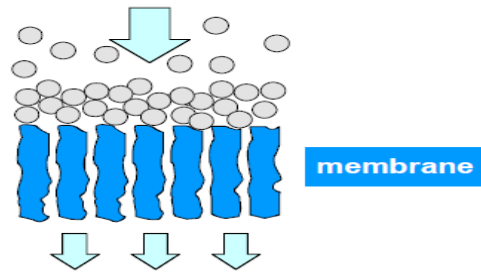
$v = \text{dynamic viscosity} [Pa/s]$

$$R_{\text{tot}} = R_{\text{mem}} + R_{\text{fouling}}$$

# Operation mode

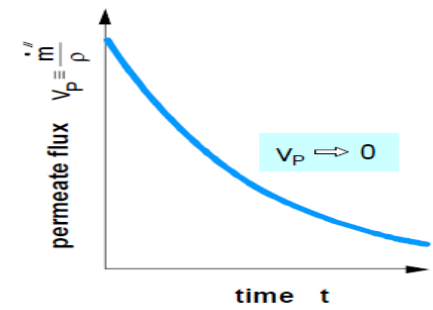
- Dead end
  - Module blocking
  - Low solid content

feed - raw water  $p_F > p_P$

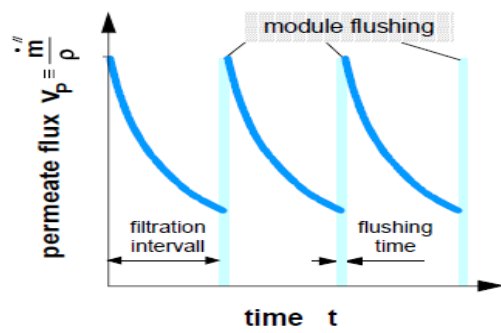


permeate - filtrate

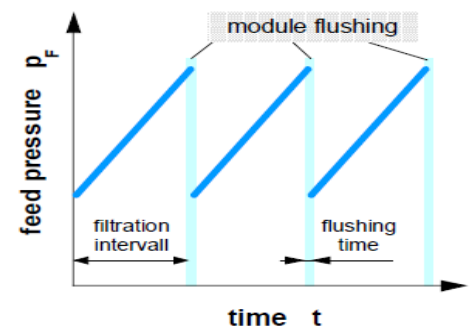
permeate flux decline



constant feed pressure  $p_F$

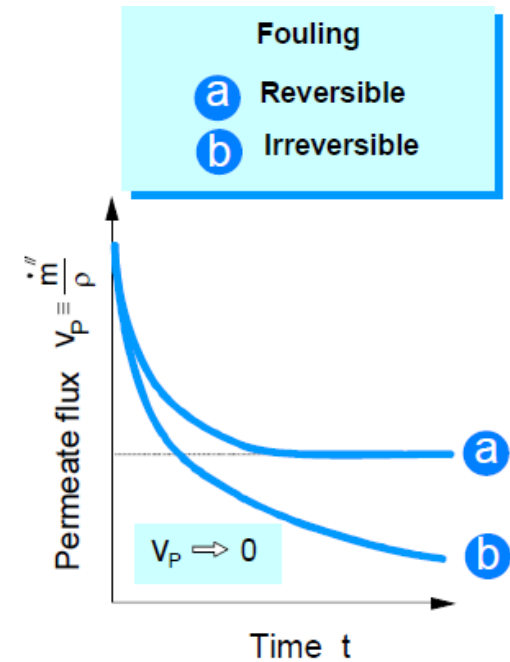
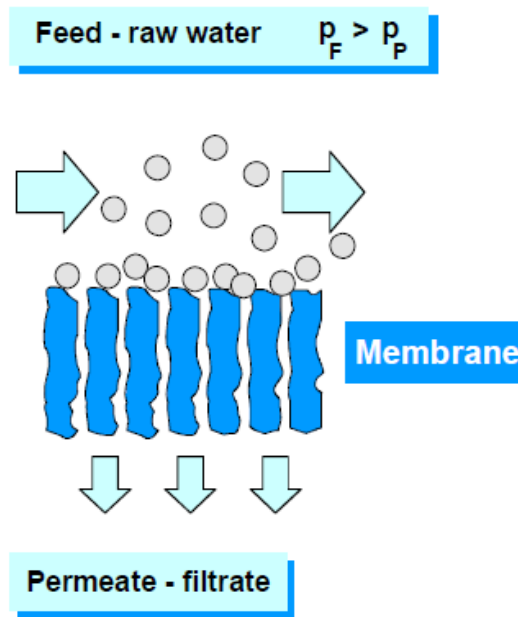


constant permeate flux  $V_p$



# Operation mode

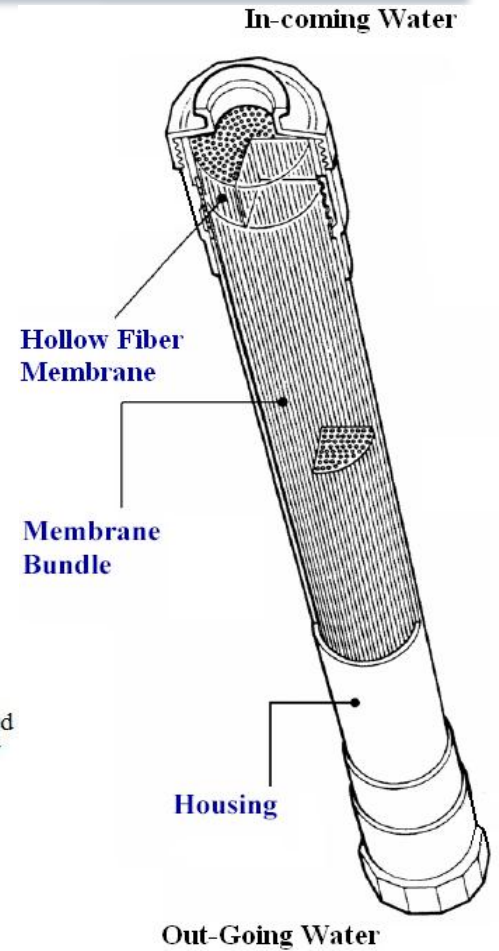
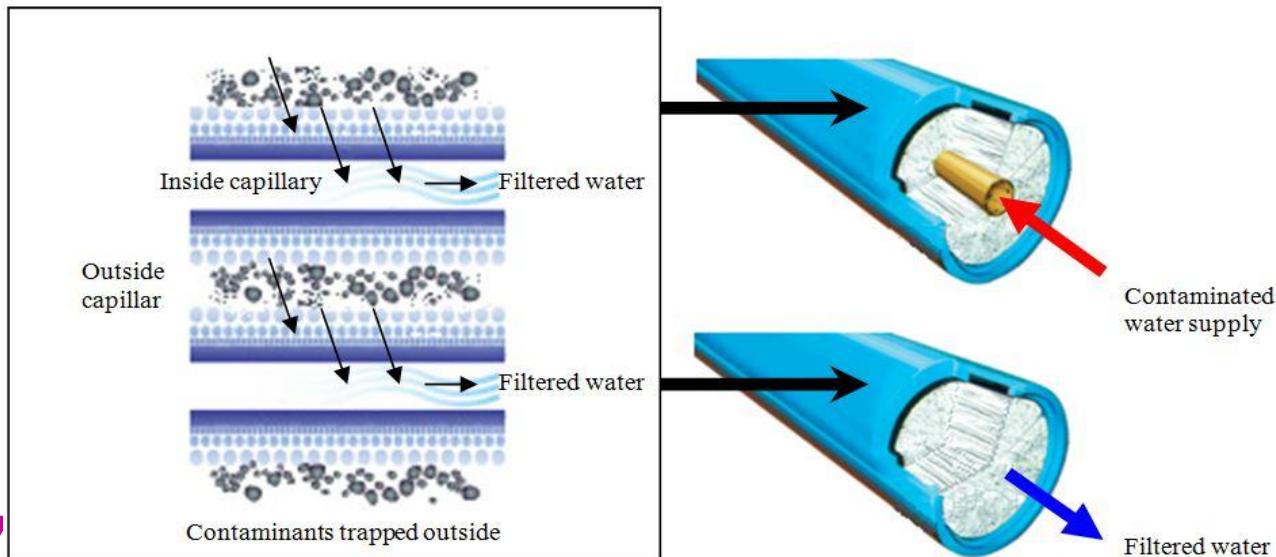
- Cross-Flow
  - High solid
  - High energy
  - High velocity





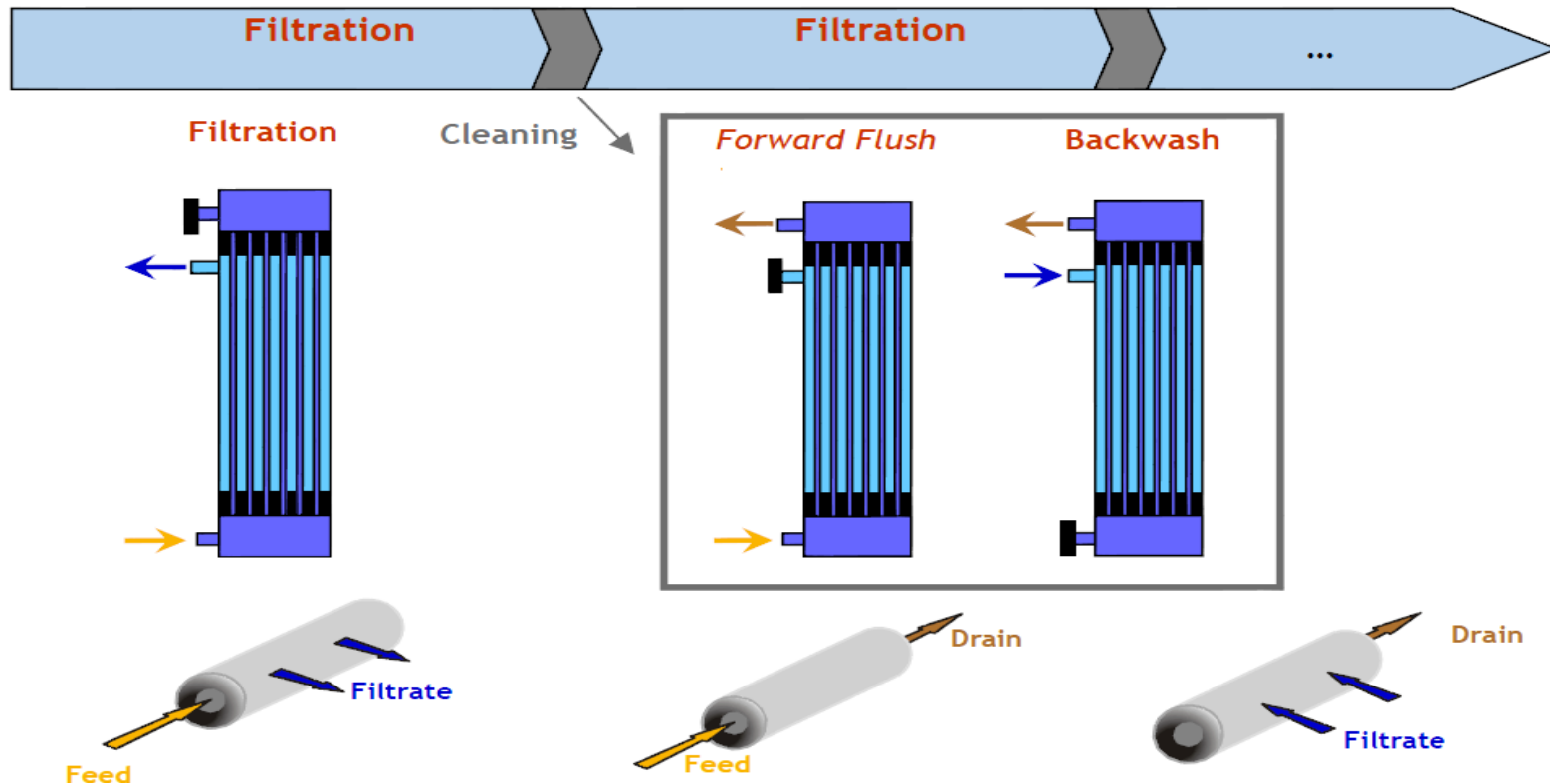
# Operation mode

- Outside-In
  - Lower plugging risks
  - Higher solids loading
  - Higher area
  - Easier cleaning



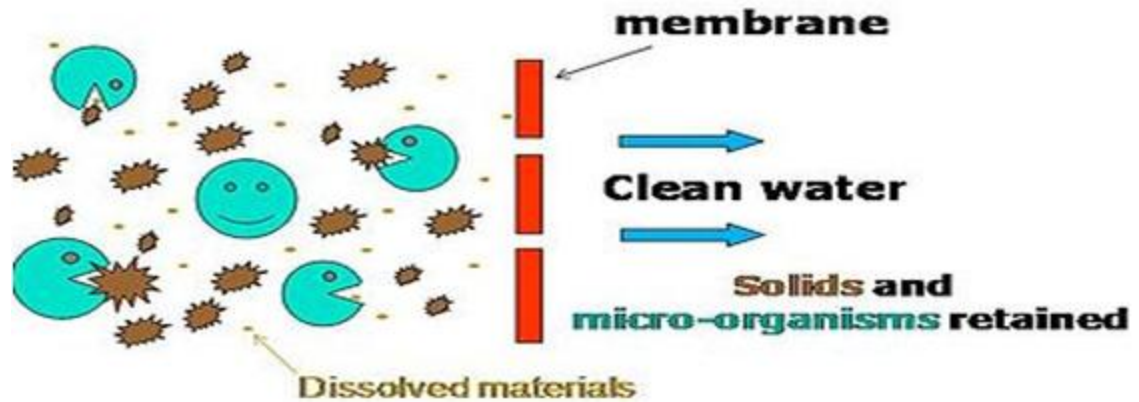
# Operation mode

- Inside-out

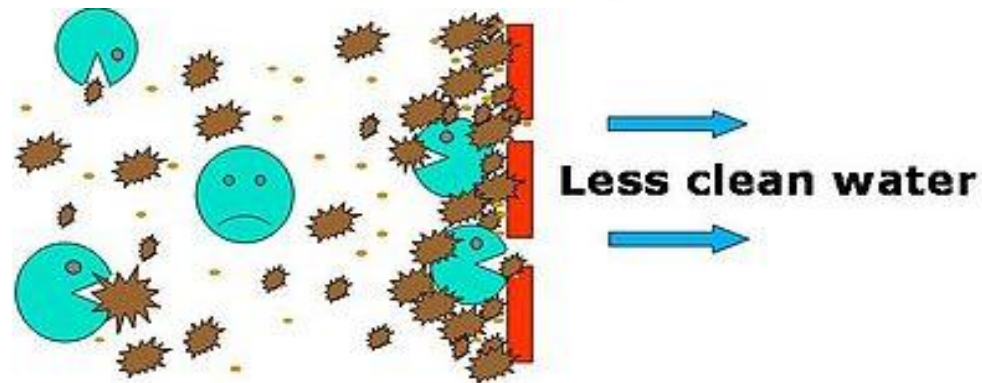


# Why UF should be cleaned?

Start-up

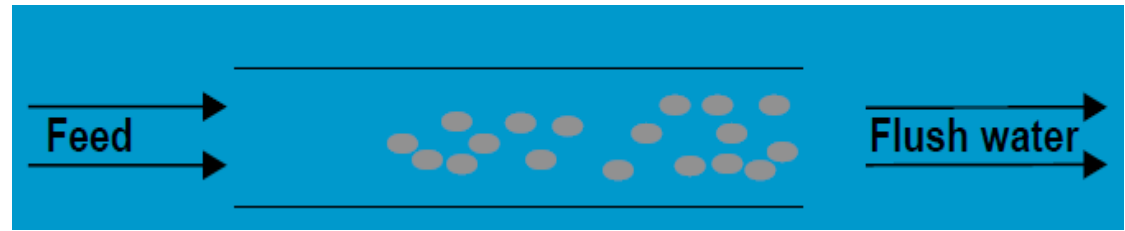


After start-up



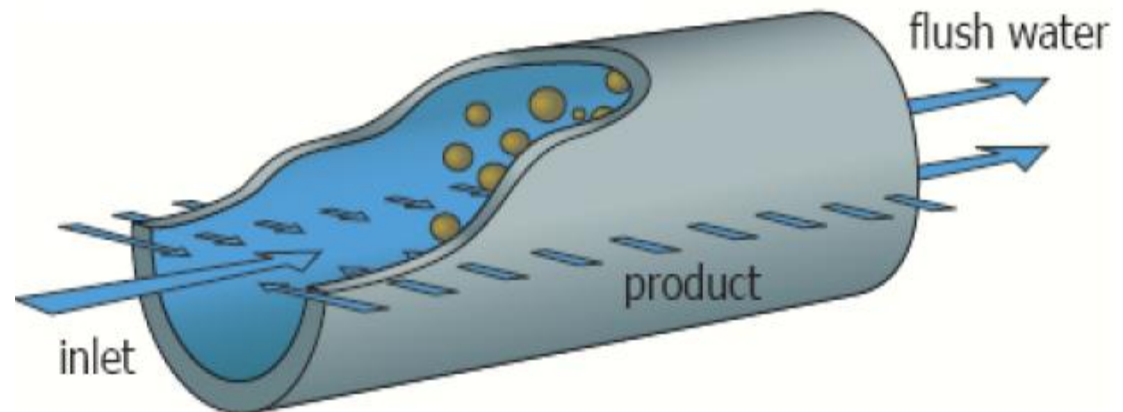
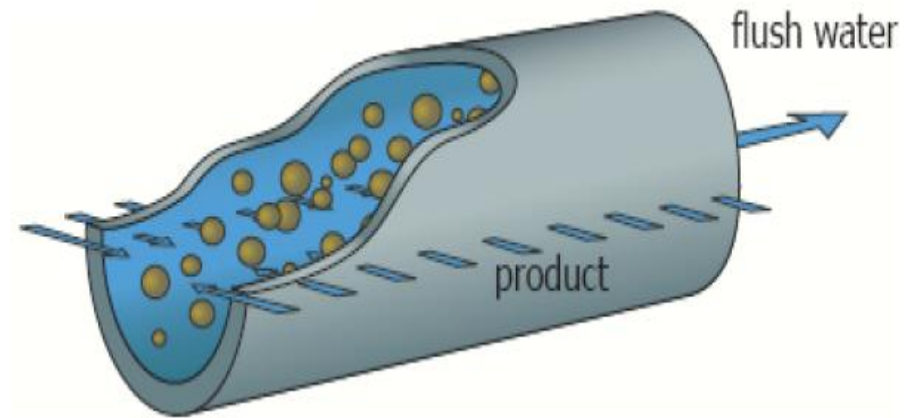
# UF cleaning

- Forward-flushing
  - Solid removal
  - Fouling reduction
- Condition
  - High velocity
  - Turbulent flow
  - Time



# UF cleaning

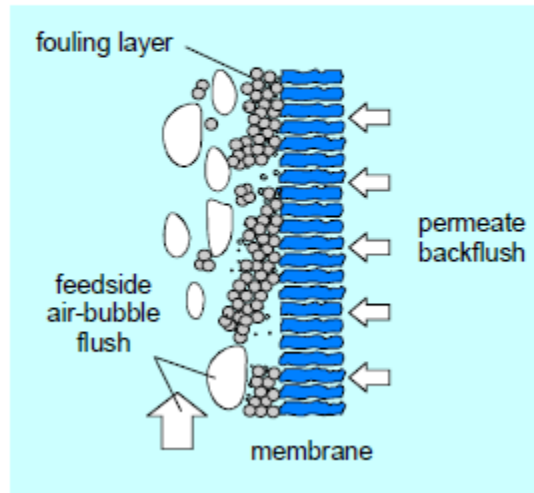
- Backward-flushing
  - Flow rate
  - Time
- Backward & forward flushing



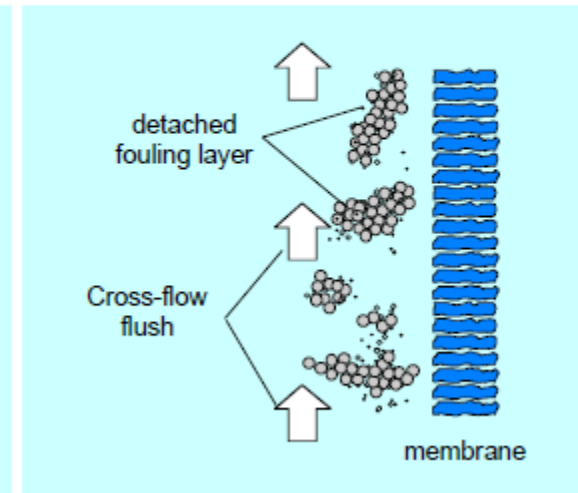
# UF cleaning

- Air flushing
  - Movement of HF
  - Shearing effect
  - Free solids removal
  
- Condition
  - Pressure
  - Flow rate
  - Time

removal of fouling layer



discharge of solids



# UF cleaning

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- Chemical cleaning
  - CEB
  - Acids&base
  - NaOCl
  - H<sub>2</sub>O<sub>2</sub>
  - Cl<sub>2</sub>
- CIP
  - Chlorines
  - Acids&base

# CSM UF membranes

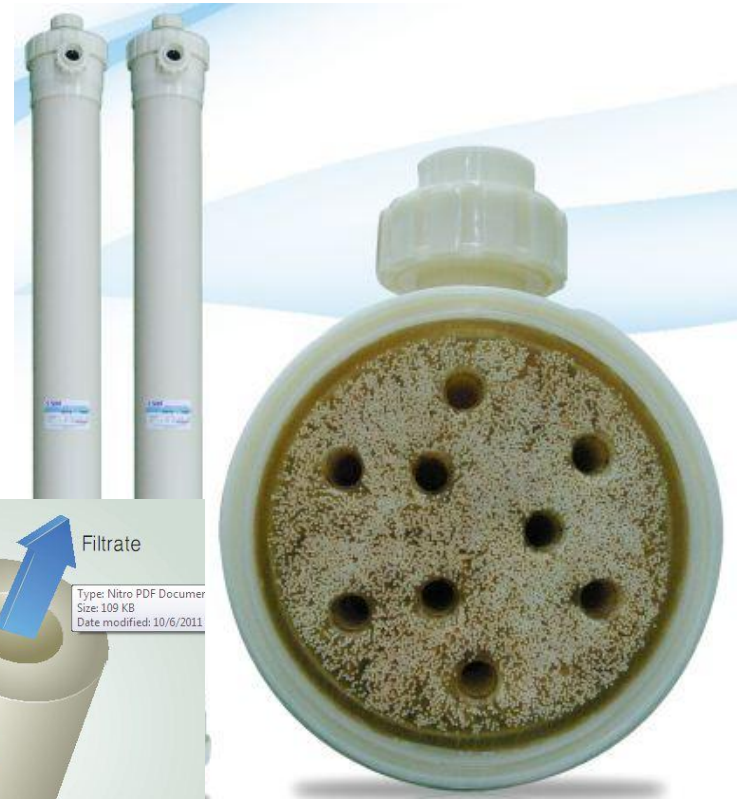
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- Spiral-wounded Module
  - PSF
  - Size: 8×40 in
  - MWCO: 50-100 kDa
  - Permeate flow rate  $\approx 52 \text{ m}^3/\text{d}$
  - Application
- Hollow Fiber Module



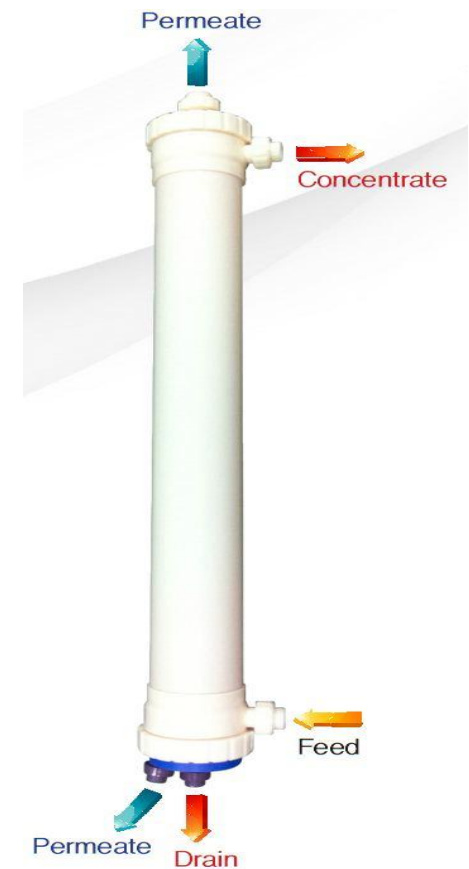
# CSM UF membranes

- High chemical resistant
  - PVDF membrane
  - Acids & base & chlorine & ...
- High mechanical resistant
- Good pore size: 0.05  $\mu\text{m}$
- Slick membrane surface
  - Low fouling
  - Microbial removal
- Out-In type
- Two-end storage type

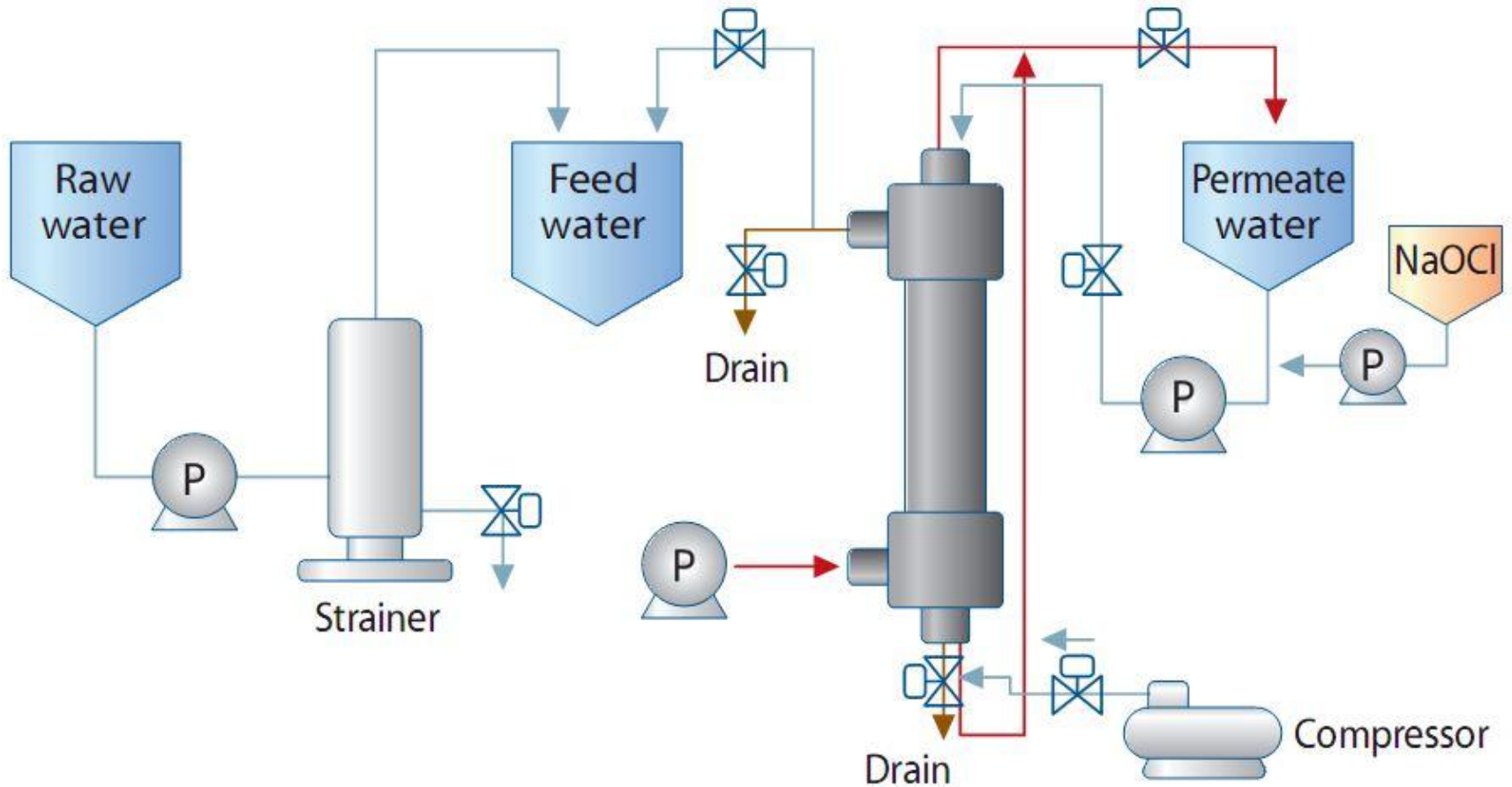


# UF module

Model		HFTS 7090
Dimension	Diameter	194 mm
	Length	2,270 mm
Effective Area		60 m <sup>2</sup>
Effective Length		1,900 mm
Material	Membrane	PVDF
	Potting	Poly-urethane
	Housing	ABS
Filtration Type		Out - in
Permeate Flow rate		1.3 ~ 5.0 m <sup>3</sup> /hr
Max. Inlet Pressure		3 kgf/cm <sup>2</sup>
Max. Operating TMP		2 kgf/cm <sup>2</sup>
Operating Temperature		1 ~ 40 °C
pH Range		2 ~ 11



# UF Plant



# Conclusion

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- Monitoring of raw water quality (turbidity, microbiology, phys.chem. Parameters, dissolved organic compounds )
- Determination of site conditions
- Applying of pre-treatment
- Pilot plant investigations
  - Membrane materials (PP, PVDF, PS, ...)
  - Size of module
  - Membrane module (cross-flow and dead-end)
  - Operating type? (out/in and in/out)
  - Optimal conditions for backwash and chemical cleaning